## fax

Shell International B.V.

Intellectual Property Services
PO Box 384
2501 CJ The Hague
The Netherlands
Tel +31 70377 2223
Fax +31 70377 6141
Email patents@shell.com
Internet http://www.shell.com

To: European Patent Office Directorate General 2 Erhardtstrasse 27 D-80298 MUENCHEN DUITSLAND

From:

Λ Krebs

Date:

04 February 2008

Your ref:

European Patent Application No. 04804628.8

Shell Internationale Research Maatschappij B.V.

Our ref:

**TS 7640 EPC P** 

Page

1 of 9

Subject:

European Patent Application No. 04804628.8

Dear Sir or Madam

Please find the enclosed letter of which a confirmation copy will follow.

Yours faithfully Shell International B.V.

A. Krebs

The material in this fax may be confidential, privileged and/or proteted by copyright. Use of this fax should be limited accordingly. If this fax has been sent to you by error, please contact us immediately.

Established at The Hague. Carol van Bylandilaan 30 Commercial Register, The Hague 27 155369

VAT number: N1004790996858

TS7640EPClaxvoorblad.doc

Shell International B.V.
Intellectual Property Services
PO Box 384
2501 CJ. The Hague
The Netherlands
Tel. +31 70377 3024
Fax +31 70377 6141
Email patents@shell.com

Internet http://www.shell.com

European Patent Office Directorate General 2 Erhardtstrasse 27 D-80298 MUENCHEN DUITSLAND

04 February 2008

Our ref:

TS 7640 EPC P

European Patent Application No. 04804628.8 Shell Internationale Research Maatschappij B.V.

Dear Sir or Madam

Please find our response to the Communication pursuant Art. 96(2) EPC (1973) in the above referred to case.

#### Amendments

We herewith submit a set of amended claims. Claim 1 has been amended, basis original claims 1 and 5. Claim 5 as originally filed has been cancelled without prejudice. Claims 6 to 14 have been renumbered accordingly. Furtehrmore, we submit an amended page 2 to replace page 2 presently on file, and a new page 2a, adding a discussion of D1.

For clarification, we refer to the amended set of claims and amended pages enclosed.

# 1. Novelty

Since claim 5 as originally filed was considered novel, amended claim 1 should be novel as well. Claims 2 to 13 are novel by virtue of their dependency on claim 1.

#### 2. Inventive step

## Inventive step in view of D2 (US-A-2003/0115857)

We consider D2, or more specifically the embodiment disclosed in Figures 3 and 4 and [0024]-[0026] as closest state of the art, since it relates to the same field (process for operating a combustion engine with exhaust gases), and since it is equally concerned with the provision of a solution to NOx abatement process.

Although both D1 and D3 have some features in common with the present invention, they are primarily concerned with the operation of a solid oxide fuel cell in an engine/fuel cell arrangement, and hence would not have formed a suitable starting point.

Eslablished at The Hague: Carel van Bylandilaan 30 Commercial Register, The Hague 27 155369 VAT number: NIO0479099658

- 2 -

### European Patent Office München

04.02.2008

The mentioned embodiment of D2 discloses a process for the catalytic exhaust gas after-treatment of engine combustion emissions by an NOx storage catalyst which can be regenerated by feeding hydrogen to the exhaust gas upstream of the NOx storage catalyst. This is achieved by operating an internal-combustion engine by a hydrocarbon fuel, such as gasoline or Diesel, which is also available to a reformer for producing a hydrogen-rich synthesis gas. The synthesis gas is then employed to drive a solid oxide fuel cell, as well as for the regeneration of a NOx storage catalyst.

The present invention differs from that disclosed in D2 in that a fuel composition comprising a Fischer-Tropsch derived hydrocarbon stream for both the compression ignition engine, as well as the catalytic partial oxidation reformer. This has the effect that less sulphur oxides will be trapped in the NOx abatement system, thereby improving performance of this system (see page 9, lines 14-19 of the present specification).

Accordingly, the objective problem in view of D2 can be formulated as to provide for a process for the operation of a combustion ignition engine with improved NOx abatement performance.

D2 does not teach or suggest use of a specific fuel, more specifically the use of a Fischer-Tropsch diesel fuel for a compression ignition engine.

Accordingly, we consider the process according to claim 1 non-obvious in view of D2.

## Inventive step in view of D2 and D1 and/or D3

D1 (US-A-2003/0168263) discloses ] a hybrid electric power train having an engine configured to produce reformate to feed a solid oxide fuel cell (see [0009]). The line-up according to D1 further comprises a start-up reformer to generate reformate until the engine supplies the fuel gas blend for the solid oxide fuel cell ([0031]). D1 further discloses in [0055] a list of considerable length of possible fuels for this line up, including "Fischer Tropsch".

Since D1 is directed mainly at a hybrid electric power train, and since it is void of any further information on how to improve the performance of the NOx abatement system through selection of engine and reformer fuel, there is no reason why a skilled person would have contemplated D1 when looking at a solution to the above problem.

However, even in the unlikely event that a skilled person would have done so, he or she would not have had any reason to select a Fischer-Tropsch fuel for use in a compression ignition engine on the basis of the teaching of D1.

D3, similar in its disclosure to D1, is fully silent about the use of a reformer to generate synthesis gas for the NOx abatement system. Although D3 discloses that a solid oxide fuel cell could operate as a reformer, this is only true for methane or methanol as fuels in the experience of Applicant.

Yet further, D3 is void of information on Fischer-Tropsch derived fuels. We therefore submit that there is no reason or suggestion that would have led a skilled person to contemplate D3, or to combine the teaching of D3 with the process of D2 when trying to solve the above problem.

- 3 -

European Patent Office München 04.02.2008

To summatise, we are of the considered opinion that the process according to claim 1 is inventive over D2, and any combination thereof with D1 and/or D3. Claims 2 to 13 are inventive by virtue of their dependency on claim 1.

Yours faithfully Shell International B.V.

A. Krcbs (GA17132)

Encls. Set of amended claims, amended page 2, new page 2a

TS 7640 EPC P

#### CLAIMS

- 1. A process for operating a compression ignition internal combustion engine in combination with a catalytic partial oxidation reformer and a  $NO_X$  abatement system as exhaust gas aftertreater, wherein:
- (a) a mixture of a first fuel and air, wherein the first fuel comprises Fischer-Tropsch derived fuel, is introduced in the combustion chamber of the engine;
- (b) exhaust gas is discharged from the engine and optionally partly recirculated to the combustion chamber of the engine;
- (c) a second fuel and oxygen and/or steam are supplied to the catalytic partial oxidation reformer to produce synthesis gas, wherein the second fuel comprises Fischer-Tropsch derived fuel;
- (d) at least part of the synthesis gas is supplied to:
- (i) the exhaust gas aftertreater;
- (ii) the combustion chamber of the engine; or to both; and wherein the non-recirculated part of the exhaust gas and at least part of the synthesis gas are supplied to the NO<sub>X</sub> abatement system.
- 2. A process according to claim 1, wherein the first fuel and the second fuel are the same fuel.
- 3. A process according to claim 1 or 2, wherein the first fuel and the second fuel comprise at least 10% (v/v) Fischer-Tropsch derived fuel, preferably at least 50% (v/v), more

Eslablished at The Hague. Carel von Bylandilaan 30 Commorcial Register, The Hague 27 155369 VAT number: N1004790996858 preferably at least 80% (v/v), even more preferably consist of Fischer-Tropsch derived fuel.

- 4. A process according to any one of the preceding claims, wherein the Fischer-Tropsch derived fuel is a gasoil.
- 5. A process according to any one of claims 1-4, wherein the  $\rm NO_X$  abatement system comprises a  $\rm NO_X$  trap comprising a  $\rm NO_X$  reducing catalyst and a  $\rm NO_X$  sorbent.
- 6. A process according to claim  $\underline{5}$ , wherein the non-recirculated part of the exhaust gas is continuously supplied to the NO<sub>X</sub> trap and the synthesis gas is intermittently supplied to the NO<sub>X</sub> trap.
- 7. A process according to claim 5, wherein the  $NO_X$  abatement system comprises two  $NO_X$  traps and wherein each trap is alternately supplied with the non-recirculated part of the exhaust gas and the synthesis gas such that one trap is supplied with the exhaust gas and the other trap with the synthesis gas.
- 8. A process according to any one of claims 1-4, wherein the  $\mathrm{NO}_{\mathrm{X}}$  abatement system comprises a  $\mathrm{NO}_{\mathrm{X}}$  reducing catalyst without a  $\mathrm{NO}_{\mathrm{X}}$  sorbent and the non-recirculated part of the exhaust gas and the synthesis gas are simultaneously and continuously supplied to the  $\mathrm{NO}_{\mathrm{X}}$  reducing catalyst.
- 9. A process according to any one of the preceding claims, wherein at least part of the synthesis gas is supplied to the combustion chamber of the engine.
- 10. A process according to any one of the preceding claims, wherein at least part of the exhaust gas is recirculated to the combustion chamber of the engine.
- 11. A process according to claim 9, wherein the amount of synthesis gas supplied to the combustion chamber of the engine

is such that the volumetric ratio of 'synthesis gas'-to-'first fuel' supplied to the combustion chamber is at most 25%, preferably at most 20%.

- 12. A process according to claim 9 and 10, wherein the amount of synthesis gas supplied to the combustion chamber and the amount of exhaust gas recirculated to the combustion chamber is such that the volumetric ratio of 'combined synthesis gas plus exhaust gas' to 'first fuel' supplied to the combustion chamber is at most 25%.
- 13. A process according to any one of the preceding claims, wherein part of the synthesis gas is supplied to a fuel cell to generate electricity, preferably a solid oxide fuel cell.

### - Amended page 2 -

- hence there is frequently observed to be a "trade-off" between  $NO_{\mathbf{x}}$  and particulate emission.

In order to reduce  $\mathrm{NO}_{\mathrm{X}}$  emissions of lean burn internal combustion engines,  $\mathrm{NO}_{\mathrm{X}}$  reducing exhaust gas treatment systems have been developed. These  $\mathrm{NO}_{\mathrm{X}}$  reducing systems typically comprise a  $\mathrm{NO}_{\mathrm{X}}$  reducing catalyst.

In US 5,412,946 for example, a  $NO_X$  reducing catalyst comprising Pt on zeolite have been described. Such a catalyst promote the reduction of  $NO_X$  to nitrogen in the presence of a reducing compound. It has been described in the art to use hydrocarbons, hydrogen or synthesis gas as reducing compound for this type  $NO_X$  reducing catalyst.

US-A-2003/0168263 discloses a hybrid electric power train having an engine configured to produce reformate to feed a solid oxide fuel cell. The line-up further comprises a start-up reformer to generate reformate until the engine supplies the fuel gas blend for the solid oxide fuel cell. The reformate is also directed to an exhaust system for regeneration of an NOx abatement catalyst in the exhaust system.

 ${
m NO}_{
m X}$  reducing systems that comprise both a  ${
m deNO}_{
m X}$  catalyst and a  ${
m NO}_{
m X}$  sorbent are also known in the art. For example from US 5,874,057, US 5,473,887 and WO 01/34950. During lean operation,  ${
m NO}_{
m X}$  is absorbed from the exhaust gas; during richer operation, the sorbent is regenerated and the catalyst promotes reduction of  ${
m NO}_{
m X}$  to nitrogen. It is disclosed that the exhaust gas can periodically be made richer (less oxygen)

Established at The Mague: Carel von Bylandilaan 30 Commercial Register, The Hague 27 155369 VAT number: NLO04790996858

### - New page 2a -

by adding fuel, hydrogen or synthesis gas to the lean exhaust gas.

An alternative method to reduce emissions of compression ignition internal combustion engines is by means of a process known in the art as fumigation. In a fumigation process, a gaseous fuel is mixed with the intake air of the engine prior to introducing the air/gaseous fuel mixture into the engine cylinder. Both diesel fuel and the air/gaseous fuel mixture are introduced into the engine. Known gaseous fuels for fumigation are for example natural gas, liquefied petroleum gas (LPG), and hydrogen gas.